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# DETERMINATION OF ACTIVITY COEFFICIENTS OF $\text{NH}_4\text{Cl}$ IN METHANOL–WATER MIXED SOLVENTS AT 25°C BY ELECTROMOTIVE FORCE MEASUREMENTS

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*(Received 30 September 2002)*

Activity coefficients of  $\text{NH}_4\text{Cl}$  in methanol–water mixtures containing respectively 0, 10, 20, 30, 40, and 50 weight percent MeOH 25°C were determined using the Pitzer ion-interaction model and the electromotive force (emf) data of the following galvanic cell without a liquid junction:  $\text{NH}_4^+ (\text{ISE}) | \text{NH}_4\text{Cl}(\text{m}), \text{H}_2\text{O} (1-x), \text{MeOH}(x) | \text{AgCl} | \text{Ag}$ . The experimental emf data were obtained using a solvent polymeric PVC ammonium selective membrane electrode containing a mixture of nonactin/monactin as ionophore and an Ag/AgCl electrode. Activity coefficients were determined over the molality range from dilute solution to near salt saturation (i.e. about 5.15 mol/kg in pure water or 2.44 mol/kg in 50% mixed MeOH–water solvent).

*Keywords:* Activity coefficient; Ammonium chloride; Ammonium-selective electrode; Mixed methanol–water solvent

## 1. INTRODUCTION

Since it has been first used in 1966 as ionophore in ion-selective electrodes (ISEs), carrier-based ion-selective solvent polymeric membranes have been shown to be useful devices, particularly, in analytical chemistry [1,2]. However, compared to cation responsive glass or solid state membrane electrodes, they were rarely [3] employed for the determination of activity coefficients in electrolytic solutions. *A fortiori*, and based on the examination of the related literature, these membranes seem to have never been used in mixed (organic–water) solvent systems for the determination of electrolytic activity coefficients. We report in the present work the results concerning the utilization of a solvent polymeric ammonium ion-selective membrane electrode for the determination of activity coefficients of  $\text{NH}_4\text{Cl}$  in mixed methanol– $\text{H}_2\text{O}$  solvents at 25°C. The investigated methanol– $\text{H}_2\text{O}$  mixed solvent systems contained 0, 10, 20, 30, 40 and 50 wt.% MeOH, respectively, in water. Activity coefficients were determined over the molality range from dilute solution to near salt saturation.

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## 2. METHOD

### 2.1. Determination of Mean Activity Coefficients ( $\gamma_{\pm}$ )

The Pitzer-interaction model has been successfully used both in aqueous solution and in mixed solvent for the determination of activity and osmotic coefficients of high concentrated pure and mixed electrolytes (e.g. [3–10]). For a single  $M_{v+}X_{v-}$  electrolyte, the Pitzer equation is written as

$$\ln \gamma_{\pm} = |z_+z_-|f^{\gamma} + m\left(\frac{2v_+v_-}{v}\right)B^{\gamma} + m^2\left(\frac{2(v_+v_-)^{3/2}}{v}\right)C^{\gamma} \quad (1)$$

where

$$f^{\gamma} = -A_{\phi}\left[\frac{\sqrt{I/m^0}}{1+b\sqrt{I/m^0}} + \frac{2}{b}\ln\left(1+b\sqrt{I/m^0}\right)\right] \quad (2)$$

$$B^{\gamma} = 2\beta^{(0)} + \frac{2\beta^{(1)}}{\alpha^2(I/m^0)}\left[1 - e^{-\alpha\sqrt{I/m^0}}\left(1 + \alpha\sqrt{I/m^0} - (1/2)\alpha^2(I/m^0)\right)\right] \quad (3)$$

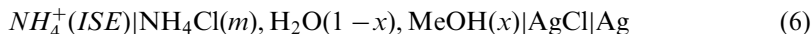
$$C^{\gamma} = (3/2)C^{\varphi} \quad (4)$$

$\gamma_{\pm}$  is the molality-scale mean ionic activity coefficient of the electrolyte  $M_{v+}X_{v-}$ ;  $Z$  the charge number of ion;  $v = v_+ + v_-$  the number of ions dissociated in one unit electrolyte formula;  $m$  the molality of electrolyte (mol/kg);  $I$  the ionic strength on a molality scale;  $\beta^{(0)}$ ,  $\beta^{(1)}$  and  $C^{\phi}$  are the parameters of the Pitzer equation;  $b = 1.2$  and  $\alpha = 2$ .  $A^{\phi}$  is the Debye-Hückel coefficient for the osmotic coefficient defined as

$$A_{\phi} = \frac{1}{3}(2\pi N_A \rho_A)^{1/2}\left(\frac{e^2}{4\pi\epsilon_0 DkT}\right) \quad (5)$$

where the constants  $\epsilon_0$ ,  $k$ ,  $N_A$ ,  $D$  and  $\rho_A$  are vacuum permittivity, Boltzmann constant, Avogadro constant, dielectric constant and density of the mixed solvent, respectively.

In this work the mean activity coefficients of  $\text{NH}_4\text{Cl}$  in methanol–water mixtures have been determined at 25°C from the electromotive force (emf) of a galvanic cell without a liquid junction combining a solvent polymeric PVC ammonium selective membrane electrode and an  $\text{Ag}/\text{AgCl}$  electrode



where  $x$  is the wt.% of MeOH in water. The emf of this cell can be represented by the Nernst relation

$$E = E' + 2s \ln(\gamma_{\pm} m) \quad (7)$$

where  $E'$  represents the cell constant potential and  $s = (RT/F)$ , in which the symbols have their usual meanings. The emf of the cell (2) was first measured at a series of electrolyte molalities in pure and mixed solvents and the root mean square deviation of  $E$ , calculated by Eqs. (1) and (3), from the measured  $E'$  was minimized by changing the value of the parameters  $\beta^{(0)}$ ,  $\beta^{(1)}$ ,  $C^{\phi}$ ,  $E'$  and  $s$  by an iteration procedure employing

the Microsoft Excel (Solver) program. The concentration of electrolyte in the cell was varied continuously by a standard addition method, by adding each time a varying volume of a concentrated stock electrolyte solution having the same solvent mixture composition as that previously utilized in the cell.

### 3. EXPERIMENTAL

#### 3.1. Reagents

Ammonium ISE membranes were prepared using high molecular poly(vinyl chloride) (PVC), mixture of nonactin (72%) and monactin (28%) as ionophore, *bis*(2-ethylhexyl)sebacate and tetrahydrofuran (THF), all of Selectophore grade from Fluka (Buchs, Switzerland). Stock solution of  $\text{NH}_4\text{Cl}$ , Microselect quality from Fluka with analytical grade (wt.%) >99.5, was prepared in triply distilled water in MeOH–water mixtures. Methanol of analytical grade (wt.%) >99.5, from Kiankavch (Iran), was fractionally distilled and only the intermediate fraction was used.

#### 3.2. Preparation of the Ammonium Membranes Electrodes

Poly(vinyl chloride) based ammonium ion-selective membrane electrodes were prepared [11–13] with the following composition (wt.%): 1.05% of the mixture of nonactin (72%) and monactin (28%), 67.07% *bis*(2-ethylhexyl)sebacate and 31.88% PVC dissolved previously in THF as a solvent. The final assembled electrodes had membranes disks with 6 mm diameters and about 200  $\mu\text{m}$  thicknesses, which were glued to PVC bodies with an outer diameter of 8 mm and inner diameter of 6 mm. The electrodes were each time back-filled for each series of measurements with 0.01 M  $\text{NH}_4\text{Cl}$  internal filling solution, in the appropriate pure water or water–MeOH mixed solvent. An Ag/AgCl wire was used as internal reference electrode.

In order to check the response of the fabricated electrode, it was initially conditioned normally for 48 h in 0.01 M  $\text{NH}_4\text{Cl}$  aqueous electrolyte solution and then calibrated using  $\text{NH}_4\text{Cl}$  test solutions, with concentration ranging from  $10^{-6}$  to 1 M [14]. A double junction Ag/AgCl electrode (Fluka, Switzerland), with 1 M lithium acetate as a bridge electrolyte, was used as an external reference. By the application of this standard procedure, with corrections for liquid junction potentials, a slope of 57.27 mV/decade change of activity) was obtained for the fabricated ammonium ISE. Ag/AgCl electrodes were prepared essentially as described elsewhere by electrolysis of Ag wire in 0.1 M HCl *versus* a Pt electrode [15]. Both ammonium and Ag/AgCl electrodes were conditioned overnight in the appropriate MeOH–water mixed solvent before each series of measurements.

#### 3.3. Emf Measurement and Data Acquisition Process

The experimental cell potentials were measured using a high input impedance (>1 G $\Omega$ ) Topward multimeter (model 1304, Taiwan, Korea) with a  $\pm 0.01$  mV resolution, interfaced with a GPIB Bus (1304G) and connected to a personal computer (32 MHz) for data acquisition and processing. All measurements were performed under stirring conditions and the temperature was kept constant at 25°C, employing a double-wall container enabling the circulation of thermostated water from a bath (Thelco, Precision

Scientific Co., USA). The electrodes and a glass thermometer ( $\pm 0.05^\circ\text{C}$ ) were immersed in the solution through a lid preventing from solvent evaporation. In each mixed solvent system and for each molality, data acquisition were performed every 4 s interval and during 20 min. From data processing a resulting final potential mean value with a standard deviation never exceeding 0.2 mV during 4 min was accepted for each concentration.

#### 4. RESULTS AND DISCUSSION

The resulted emf values of the cell (6) and the calculated mean activity coefficients of  $\text{NH}_4\text{Cl}$  electrolyte in different mixed MeOH–water solvent systems at  $25^\circ\text{C}$  are reported in Table I. The variation of natural logarithm of  $\text{NH}_4\text{Cl}$  mean activity coefficient *versus*

TABLE I The emf *versus* molality and the corresponding mean activity coefficients for  $\text{NH}_4\text{Cl}$  in various (wt.%) mixed MeOH–water solvent systems, at  $25^\circ\text{C}$

| <i>m</i> (mol/kg) | <i>E</i> (mV) | $\gamma_{\pm}$ | <i>m</i> (mol/kg) | <i>E</i> (mV) | $\gamma_{\pm}$ | <i>m</i> (mol/kg) | <i>E</i> (mV) | $\gamma_{\pm}$ |
|-------------------|---------------|----------------|-------------------|---------------|----------------|-------------------|---------------|----------------|
| 0 wt.% wt. MeOH   |               |                | 10 wt.% wt. MeOH  |               |                | 20 wt.% wt. MeOH  |               |                |
| 0.0018            | −84.4         | 0.9536         | 0.0014            | −69.8         | 0.9561         | 0.0009            | −114.9        | 0.9596         |
| 0.0051            | −33.7         | 0.9259         | 0.0029            | −38.5         | 0.9375         | 0.0028            | −64.8         | 0.9329         |
| 0.0127            | 10.6          | 0.8904         | 0.0087            | 5.1           | 0.8990         | 0.0074            | −20.0         | 0.8961         |
| 0.0255            | 43.9          | 0.8550         | 0.0212            | 40.3          | 0.8544         | 0.0170            | 16.7          | 0.8536         |
| 0.0378            | 62.5          | 0.8319         | 0.0336            | 58.2          | 0.8264         | 0.0265            | 36.2          | 0.8257         |
| 0.0993            | 107.2         | 0.7668         | 0.0899            | 95.7          | 0.7563         | 0.0732            | 79.7          | 0.7497         |
| 0.2180            | 143.0         | 0.7081         | 0.1938            | 124.2         | 0.6947         | 0.1628            | 113.0         | 0.6809         |
| 0.4407            | 174.7         | 0.6554         | 0.3845            | 149.4         | 0.6388         | 0.3305            | 141.8         | 0.6174         |
| 0.6470            | 192.0         | 0.6284         | 0.5605            | 163.2         | 0.6092         | 0.4852            | 157.3         | 0.5837         |
| 1.0179            | 212.5         | 0.5998         | 0.8713            | 179.4         | 0.5769         | 0.7614            | 175.5         | 0.5460         |
| 1.4179            | 227.8         | 0.5822         | 1.1965            | 191.1         | 0.5561         | 1.0565            | 188.7         | 0.5208         |
| 2.0603            | 245.4         | 0.5672         | 1.7156            | 204.6         | 0.5361         | 1.5218            | 203.7         | 0.4958         |
| 2.7582            | 259.5         | 0.5602         | 2.2732            | 215.4         | 0.5239         | 2.0183            | 215.4         | 0.4794         |
| 3.3966            | 269.8         | 0.5580         | 2.7753            | 223.3         | 0.5174         | 2.4631            | 223.9         | 0.4696         |
| 4.0136            | 278.3         | 0.5580         | 3.2550            | 229.6         | 0.5137         | 2.8861            | 230.7         | 0.4630         |
| 4.5172            | 284.3         | 0.5589         | 3.6406            | 234.2         | 0.5117         | 3.2264            | 235.6         | 0.4590         |
| 4.9009            | 288.5         | 0.5597         | 3.9345            | 237.3         | 0.5107         | 3.4828            | 238.9         | 0.4566         |
| 5.1479            | 291.1         | 0.5603         | 4.1222            | 239.2         | 0.5102         | 3.6463            | 241.0         | 0.4552         |
|                   |               |                | 4.2202            | 240.2         | 0.5100         | 3.6720            | 241.3         | 0.4550         |
| 30 wt.% wt. MeOH  |               |                | 40 wt.% wt. MeOH  |               |                | 50 wt.% wt. MeOH  |               |                |
| 0.0009            | −68.7         | 0.9568         | 0.0007            | −48.0         | 0.9565         | 0.0007            | −208.9        | 0.9523         |
| 0.0024            | −39.1         | 0.9304         | 0.0015            | −29.5         | 0.9397         | 0.0020            | −173.8        | 0.9209         |
| 0.0061            | −12.7         | 0.8950         | 0.0037            | −5.3          | 0.9083         | 0.0054            | −142.5        | 0.8770         |
| 0.0155            | 13.5          | 0.8445         | 0.0074            | 12.6          | 0.8758         | 0.0123            | −117.3        | 0.8268         |
| 0.0247            | 26.2          | 0.8135         | 0.0074            | 12.6          | 0.8758         | 0.0187            | −104.6        | 0.7952         |
| 0.0708            | 54.4          | 0.7286         | 0.0366            | 52.8          | 0.7650         | 0.0505            | −75.3         | 0.7050         |
| 0.1568            | 74.9          | 0.6544         | 0.0723            | 69.1          | 0.7026         | 0.1082            | −53.9         | 0.6237         |
| 0.3149            | 92.5          | 0.5867         | 0.1416            | 84.7          | 0.6346         | 0.2182            | −35.1         | 0.5437         |
| 0.4577            | 101.8         | 0.5509         | 0.1416            | 84.7          | 0.6346         | 0.3096            | −25.9         | 0.5034         |
| 0.7114            | 112.7         | 0.5104         | 0.2715            | 99.4          | 0.5654         | 0.4646            | −15.6         | 0.4571         |
| 0.9807            | 120.6         | 0.4830         | 0.3326            | 103.9         | 0.5437         | 0.6395            | −7.6          | 0.4216         |
| 1.4054            | 129.6         | 0.4549         | 0.6043            | 116.9         | 0.4807         | 0.9909            | 3.1           | 0.3749         |
| 1.8582            | 136.7         | 0.4357         | 0.8306            | 123.7         | 0.4484         | 1.3642            | 10.8          | 0.3428         |
| 2.2632            | 141.7         | 0.4238         | 1.0219            | 128.1         | 0.4280         | 1.6835            | 15.8          | 0.3226         |
| 2.6529            | 145.8         | 0.4152         | 1.3277            | 133.6         | 0.4033         | 1.9754            | 19.6          | 0.3078         |
| 2.9595            | 148.7         | 0.4099         | 1.5613            | 137.0         | 0.3886         | 2.2011            | 22.1          | 0.2981         |
| 3.1923            | 150.7         | 0.4065         | 1.7456            | 139.4         | 0.3788         | 2.3678            | 23.8          | 0.2916         |
| 3.3313            | 151.9         | 0.4046         | 1.7456            | 139.4         | 0.3788         | 2.4720            | 24.8          | 0.2879         |
|                   |               |                |                   |               |                | 2.4899            | 25.0          | 0.2873         |

the square root of electrolyte molality in water and various wt.% MeOH–water mixed solvent are also illustrated in Fig. 1. Pitzer interaction parameters, computed by the minimization procedure for these systems are, as well, given in Table II. For the constants  $b$  and  $\alpha$ , the values  $b=1.2$  and  $\alpha=2$  were used according to Koh *et al.* [6], who showed that these values, defined for aqueous systems, are still appropriate for

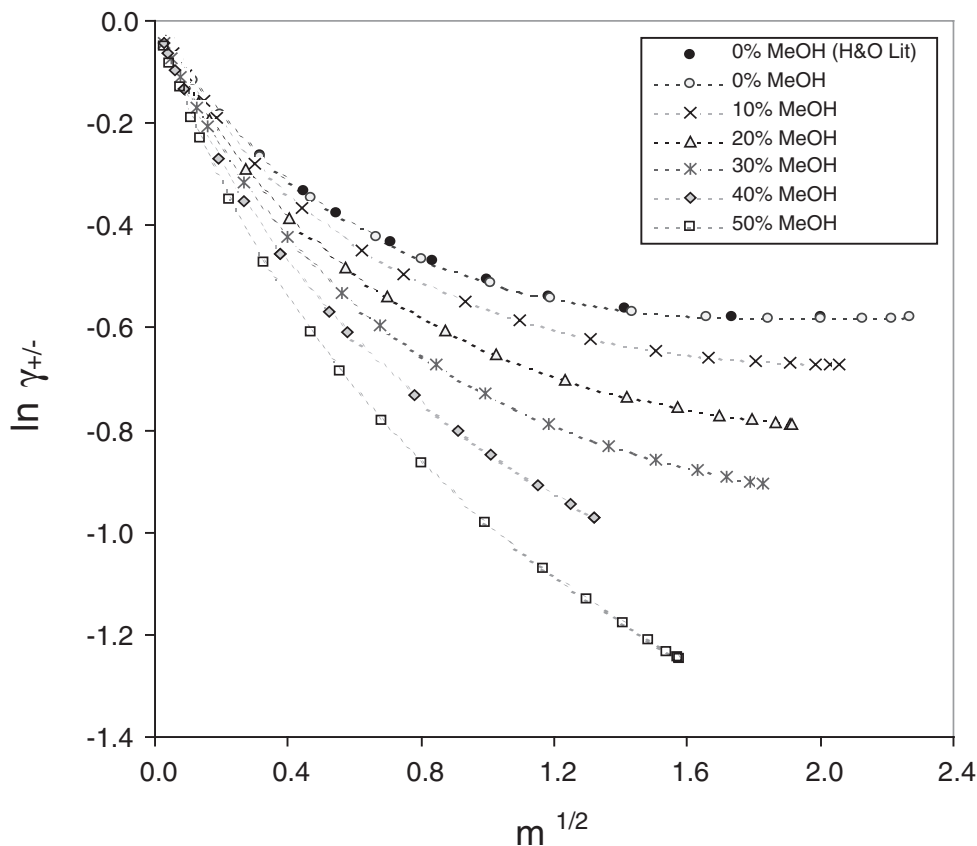


FIGURE 1 Natural logarithm of mean activity coefficient of NH<sub>4</sub>Cl versus square root of molality in various mixed wt.% MeOH–water solvent systems, at 25°C. The corresponding literature data in pure water solvent at 25°C are those reported by Harned and Owen [17].

TABLE II Values obtained for Pitzer parameters, dielectric constant ( $D$ ), density ( $\rho_A$ ) and Debye-Hückel coefficients for the osmotic coefficient ( $A_\phi$ ), for NH<sub>4</sub>Cl at different wt.% of MeOH–water at 25°C

| MeOH x%<br>(wt.) | $\beta(0)$ | $\beta(1)$ | $C^\phi$ | $A_\phi$ | $D$   | $\rho_A$<br>(g/cm) <sup>3</sup> |
|------------------|------------|------------|----------|----------|-------|---------------------------------|
| 0 <sup>a</sup>   | 0.05192    | 0.19346    | -0.00298 |          |       |                                 |
| 0                | 0.05188    | 0.19356    | -0.00299 | 0.3915   | 78.54 | 0.997                           |
| 10               | 0.05118    | 0.19362    | -0.00302 | 0.4229   | 74.10 | 0.983                           |
| 20               | 0.05020    | 0.19389    | -0.00298 | 0.4661   | 69.18 | 0.967                           |
| 30               | 0.04970    | 0.19455    | -0.00292 | 0.5147   | 64.30 | 0.951                           |
| 40               | 0.03491    | 0.19487    | -0.00278 | 0.5618   | 59.55 | 0.934                           |
| 50               | 0.03090    | 0.20361    | -0.00305 | 0.6382   | 54.90 | 0.916                           |

<sup>a</sup>The values of Pitzer parameters reported by Marshall *et al.* [18] for NH<sub>4</sub>Cl in pure water at 25°C.

TABLE III The resulting fitted values of the  $a$ ,  $b$ ,  $c$ ,  $d$ ,  $e$  and  $f$  constants employed in the non-linear power series equation (8) used successively for the determination of  $A_\phi$ , dielectric constant ( $D$ ) and density ( $\rho_A$ ), at different wt.% of mixed MeOH–water solvent systems at 25°C

|     | $A_\phi$  | $D$       | $\rho_A$<br>(g/mL) |
|-----|-----------|-----------|--------------------|
| $a$ | -2.23E-10 | 1.52E-08  | 4.94E-11           |
| $b$ | 5.14E-08  | -3.28E-06 | -1.05E-08          |
| $c$ | -3.44E-06 | 2.48E-04  | 7.19E-07           |
| $d$ | 1.25E-04  | -7.79E-03 | -2.37E-05          |
| $e$ | 2.28E-03  | 0.3878    | -1.22E-03          |
| $f$ | 0.3906    | 78.54     | 0.997              |

MeOH–water mixed solvents systems. The utilized values of  $A_\phi$ , dielectric constant and density for different solvent compositions are also included in Table II. These constants were obtained from discrete values from the literature [16,17] that have been fitted perfectly ( $R^2 \approx 1$ ) to the following non-linear power series equation

$$y = ax^5 + bx^4 + cx^3 + dx^2 + ex + f \quad (8)$$

where  $y$  represents successively:  $A_\phi$ , dielectric constant ( $D$ ) or density ( $\rho_A$ ) in the corresponding composition of the mixed solvent system, and  $x$  the wt.% of methanol in the mixed MeOH–water solvent systems. Table III shows the obtained values of the  $a$ ,  $b$ ,  $c$ ,  $d$ ,  $e$  and  $f$  constants successively for  $A_\phi$ , dielectric constant ( $D$ ) and density ( $\rho_A$ ) for different solvent compositions.

Only the results obtained for  $\text{NH}_4\text{Cl}$  in pure water could be compared with the corresponding available literature data. Figure 1 shows that the obtained values of mean activity coefficient for  $\text{NH}_4\text{Cl}$  match well with those previously reported in pure water [17]. Similarly, Table II shows that the obtained values of the Pitzer interaction parameters for  $\text{NH}_4\text{Cl}$  electrolyte in pure water solvent are also very close to those reported in the literature [18].

## 5. CONCLUSION

The results concerning the use of a solvent polymeric ammonium ion-selective membrane electrode for the determination of activity coefficients of  $\text{NH}_4\text{Cl}$  in mixed methanol– $\text{H}_2\text{O}$  solvents at 25°C, using the Pitzer ion-interaction model and the electromotive force (emf) data of a galvanic cell without a liquid junction were reported. The used mixed solvent systems contained 0, 10, 20, 30, 40 and 50 wt.% MeOH, respectively, in water. Activity coefficients were determined over the molality range from dilute solution (i.e. about 0.0018 mol/kg in pure water) to near salt saturation (i.e. about 5.15 mol/kg in pure water or 2.44 mol/kg in 50% mixed MeOH–water solvent). A non-linear (5th order) power series equation was also presented for the determination of  $A_\phi$ , dielectric constant and density for different compositions of mixed MeOH–water solvent. The resulted values of mean activity coefficient as well as the values of Pitzer interaction parameters obtained for  $\text{NH}_4\text{Cl}$  compared well with those previously reported in pure water [17,18]. This satisfactory agreement

between our results, which are obtained in a more extended concentration range than those reported in the literature for pure water solvent [17], confirms the reliability of our results in mixed solvent systems.

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